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A process for the synthetic generation of methane

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Description

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A process for the synthetic generation of methane

The invention relates to a process for the synthetic generation of methane from a feed gas mixture comprising carbon monoxide, hydrogen and water vapour and optionally aromatic hydrocarbons.

Even there does not exist actually a distinct proof for the greenhouse effect and accordingly the global warming, it is the intention of the world-wide community to reduce the production of gaseous climate relevant components, such as chlorofluorocarbons (CFC) and carbon dioxide. For the reduction of the CFC's significant process has been achieved in the recent years since its production has been worldwide downsized to almost zero. For the carbon dioxide the worldwide community committed itself to reduce the production within the next decade in the range of about 10 to 15%, depending on the country and its commitment to the Kyoto agreement.

For instance, Switzerland committed itself to reduce the production of carbon dioxide originating from traffic related combustion processes by 8% until 2012. Even under an optimistic consideration, it is most unlikely that this ambitious target will be met. As a possible alternative, so-called biofuels have the potential to influence the carbon dioxide balance tremendously on a midterm and long-term basis as being a relevant source for renewable primary products, such as wood or related biomass. The estimated cost are expected in the range of 300 Swiss Francs per ton of CO₂. This cost are compared to other options taken in the transportation sector quite un-expensive.

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Beside the effect of the efficient reduction of carbon dioxide the aspect of growing the independency from the crude oil syndicates led to an increasing focus on biofuels. The commission of the EU intends to gain in the year 2020 at least 5 20% of the consumed fuel from alternative fuels. Beside natural gas (methane) and hydrogen the biofuels are categorized as potential alternative. On a short-term basis fuels like RME (bio diesel), ethyl alcohol and bio gas, are available; in midterm and long-term range, bio methyl alcohol 10 and so-called Fischer-Tropsch fuel shall be produced according to the already theoretically well-known thermo-chemical processes which takes advantage of an catalyst in order to transform a synthesis gas into the desired bio fuel, such as methyl alcohol, gasoline, diesel, methane and hydrogen.

15

A most promising fuel is methane that is supplied actually as fossile gas and which can be replaced under efficient use of synergies between the required infrastructure for both the fossile gas and the biogen gas by the latter that can be 20 produced by fermentation as well as by thermo-chemical processes.

Unfortunately, one of the most preferred renewable primary product, wood, can not be transformed into bio gas by 25 fermentation. Therefore, it is an crucial task to provide efficient alternative processes for the synthetic generation of methane. Such processes are under intensive R&D activities in the scientific and economical world and some of the process have been revealed as being practicable, even under severe 30 economical considerations.

A process known in the art uses wood in a gasification reactor, such as FICFB (*Fast Internally Circulation Fluidized Bed*), which requires subsequently non-negligible efforts for 35 the pretreatment of the raw synthesis gas in order to allow both effective and efficient synthesis of methane. As far as wood is considered as the renewable primary product, it has to

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be pointed out that the raw synthesis gas originating from the gasification step, is loaded with considerable amounts of aromatic hydrocarbons which are known in the prior art to deploy a negative impact in the subsequent process chain.

- 5 Therefore, the removal of these aromatic hydrocarbons, such as benzene, toluene and naphthaline (BTN), is acknowledged as being a required process requisite prior to a subsequent removal of ammonia NH_3 and hydrosulfide H_2S . Unfortunately, these additional process requisites tend to increase the cost
- 10 of the synthetic generation of methane from wood, which is an almost exhaustless renewable primary product and reduces the overall efficiency.

- For the reason given above, the crucial pre-requisite for a commercialized exploitation of wood and other biomasses for
- 15 the synthetic generation of methane is to find an optimized concert between the processes of gasification, raw synthesis gas purification, methane generation and catalyst properties which is required in the methane generation.

- 20 Accordingly, it is the aim of the invention to provide a process which allows the synthetic generation of methane for a renewable primary product, explicitly including wood and related materials, in an economically and commercially
- 25 reasonable manner.

- This aim is achieved according to the invention by a process for the synthetic generation of methane from a feed gas mixture, i.e. a feed gas mixture originating from a biomass
- 30 gasification process, comprising carbon monoxide, hydrogen and water vapour and optionally aromatic hydrocarbons; said process comprising the steps of:

- a) bringing the feed gas mixture in contact with a fluidized bed catalyst having catalyst particles which comprise as
- 35 catalytic active component a metal and/or a metal compound or a mixture thereof;

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under the circumstances of:

- b) an elevated temperature in the range of 250 to 500°C;
- c) a feed gas pressure in the range of 0.8 to 70 bar;
- d) an gas hourly space velocity of 1000 to 50000 h⁻¹; and
- 5 e) an concentration of H₂/CO in the feed gas mixture in the range of 0.25 to 5.

The afore-mentioned process allows to catalytically convert hydrogen and carbon monoxide effectively in the fluidized bed catalyst which avoids an advanced deactivation of the catalyst material and therefore delivers a high activity of the catalytic active components in the process. Both thermo-chemical reactions, the endothermic reformation of higher hydrocarbons, i.e. aromatic hydrocarbons, and the exothermic methane generation, themselves synergetically fertilize which in fact tremendously increases the tolerance of this process against the content of higher hydrocarbons in the feed gas mixture, such a the raw synthesis gas of a wood gasification process, by simultaneously enhancing the robustness of the catalytic activity of the catalyst particles.

With respect to the initial and continuing catalytic activity, excellent results have been achieved by using as catalytically active component nickel and/or a nickel compound, preferably a mixture of nickel and nickel monoxide, disposed on an ceramic carrier, such as Al₂O₃, TiO₂, SiO₂ or Y₂O₃ or mixtures thereof. Additionally, the content of the catalytically active component may be in the range of 20 to 80 weight%, preferably 40 to 60 weight%, as compared to the weight of the catalyst particles. A suitable catalyst may comprise nickel and nickel oxide disposed on alumina (Al₂O₃) having a content of the catalytically active component in the range of 50 weight% as calculated as neat nickel.

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In order to achieve both a high mobility of the catalyst particles in the fluidized bed catalyst and a sufficient BET surface, the size of the catalyst particles may be in the
5 range of 10 to 1000 μm , preferably in the range of 100 to 500 μm .

With respect to the energy balance of the exothermic generation of methane an advantageous feed gas composition is
10 considered to have a positiv impact thereupon when the feed gas mixture comprises aromatic hydrocarbons, such as benzene, toluene and naphthalene, in the range of less than 10 Vol%, preferably less than 5 vol%. Explicitly, this gas composition covers broadly a synthesis gas that originates from wood ...
15 gasification processes to which a major focus is laid upon due to the environmental demands.

A superior yield with respect to the generation of methane as well as to a complete conversion of the higher hydrocarbons
20 may require that the gas hourly space velocity (GHSV) is in the range of 2000 to 10000 h^{-1} , the temperature is in the range of 340 to 400°C and the gas pressure is in the range of 1? Ausführungsbeispiel? bar. With respect to the above-mentioned nickel/nickel oxide catalyst, the temperature is preferably in
25 the range of 350°C, the GHSV in the range of 4200 h^{-1} and the pressure is ambient pressure.

In order to offer ambient condition in the fluidized bed catalyst that supports both the catalytic reactions of
30 reforming higher hydrocarbons and formation of methane and the regeneration of the catalyst particles, a mean residence time of the feed gas mixture in the fluidized bed catalyst may range from 0.1 to 5 sec., preferably 0.2 to 1 sec.

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Again with respect to the yield of methane and to the reformation of higher hydrocarbons the content of H_2/CO in the feed gas mixture is in the range of 0.8 to 3, for example in the range of 1.5 as combined with the afore-mentioned nickel/nickel oxide catalyst.

Exemplarily embodiments of the inventive process are described in detail below without the intention to limit the invention to these actually preferred examples.

The measurements were taken with a plant as shown schematically below in Figure 1. The measurement campaign can be divided in three different sections:

15

Phase 1: The feed gas mixture is pretreated with a washer unit and an activated carbon filter (charcoal absorber);

20

Phase 2: The feed gas mixture is now only pretreated with the washer unit; and

Phase 3: The feed gas mixture is taken as of the outlet of the wood gasification.

25

Especially for the intention of maintaining the activity and selectivity of the catalyst, unsaturated hydrocarbons (such as C_2H_4 , C_2H_2), light tar components (such as benzene, toluene, naphthaline, C8: phenylacetylene, styrole, indene) and ammonia are considered to highly disturb these demands.

30

Figure 1 shows that the complete plant comprise an inlet at 1) for the feed gas mixture originating from a non-illustrated wood gasification unit, followed by a washer unit at 2), an activated carbon filter at 3), a gas pump and the respective unit COALA for the generation of methane which is observed at

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the outlet of COALA at 4). The methane generation unit COALA comprises a desulphurisation unit in form of a ZnO fixed bed catalyst, an inlet for the supply of water vapour, a fluidized bed catalyst, a filter and a heat exchanger as seen in
5 direction of the gas flow.

In phase 1, the washer unit for the removal of ammonia NH_3 and the activated carbon filter for the removal of higher hydrocarbon are disposed upstream the COALA. The gas
10 composition during the first 40 hours of service is given in table 1; the first line giving the data for the gas composition upstream the activated carbon filter, second and third line the respective gas compositions downstream the activated carbon filter after 3 and 40 h of service, resp.

15

Table 2 gives the gas compositions in phase 1 with respect to benzene, toluene, naphthaline and C8 at the probe locations 1), 2), 3) and 4). Almost all disturbing higher hydrocarbons are already removed at 3) grace to both the washer unit and
20 the activated carbon filter. The plant was operated continuously at a temperature of about 360°C , a water content of 0.25 as related to the dry gas volume and a gas volume flow rate of $0,6 \text{ m}^3/\text{h}$.

25 During phase 2, the plant was operated without activated carbon filter and the gas composition with respect to higher hydro carbons is given in table 3.

During phase 3, the plant was operated without any
30 pretreatment of the feed gas mixture. As already before in phases 1 and 2, for the fluidized bed catalyst 100 g catalyst particles having a size of $200 \mu\text{m}$ and comprising an even content of nickel and nickel oxide supported by alumina (Al_2O_3) whereby the content of the catalytically active nickel
35 components is 50 weight% as calculated as neat nickel, was used. The gas composition for the higher hydrocarbons is given in table 4. At the entrance the average load of benzene,

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toluene, naphthaline and C8 was in the range of 13.6 g/Nm³
resp. 0.6 g/Nm³ resp. 0.8 g/Nm³ resp. 0.5 g/Nm³. At the outlet
at 4) these higher hydrocarbons were reformed almost
completely without the occurrence of any catalyst deactivation
5 or loss in selectivity.

The comparison data given in table 5 is in so far self-
explanatory, when the following definitions are observed:

10 The steam/dry gas ratio

$$D_V = \frac{n_{H_2O}}{n_{Gas\ tr.}} \quad [-]$$

and the catalyst load

15

$$KB = \frac{n_{Gas\ tr} + n_{H_2O}}{M_{Kat}} \quad \left[\frac{\text{mol}}{\text{kg} \cdot \text{h}} \right]$$

originating from the generation of methane from synthesis gas,
such as pure H₂/CO gas. The „steam to carbon ratio“

20

$$S/C = \frac{n_{H_2O}}{n_{Carbon}} \quad [-]$$

is known from the steam reforming of methane. All above
mentioned key figures are used in a sense that clearly
25 determined distinct gas compositions were used. Therefore,
they are not sufficient in order to describe the process of
generating methane from a synthesis gas being achieved by a
biomass gasification process. Additionally, the H/C ratio in
both a dry product gas

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$$H/C_r = \frac{n_H}{n_C}$$

as well as in a humidified product gas

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$$H/C_f = \frac{n_H + 2 \cdot n_{H_2O}}{n_C}$$

is a suitable parameter to characterize the process properly.

- 5 A further meaningful parameter is the conversion rate of carbon monoxide

$$U_{CO} = \frac{n_{COin} - n_{COout}}{n_{COin}} \quad [-],$$

- 10 the selectivity to methane

$$S_{CH_4} = \frac{n_{CH_4in} - n_{CH_4out}}{(n_{COin} - n_{COout}) + X \cdot (n_{C_2H_4in} - n_{C_2H_4out})} \quad [-]$$

and the so called cold gas efficiency,

15

$$\eta_{KG} = \frac{\text{Heat value}_{CH_4out}}{\text{Heat value}_{in}}$$

which describes the thermal power at the outlet with respect to the output of methane in relation to the overall thermal power at the inlet.

20

Surprisingly, the catalyst does not show any effect of deactivation and/or loss in selectivity what is indicated by the data given in the third and forth line. The third line stands for the results in a phase 3a during the initial hours of operation. The results in the forth line stand for the gas compositions that have been achieved by continuously operating the plant over dozens of hours.

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Patent Claims

1. A process for the synthetic generation of methane from a feed gas mixture comprising carbon monoxide, hydrogen and water vapour and optionally aromatic hydrocarbons; said process comprising the steps of:

- a) bringing the feed gas mixture in contact with a fluidized bed catalyst having catalyst particles which comprise as catalytic active component a metal and/or a metal compound or a mixture thereof under the circumstances of:
- b) an elevated temperature in the range of 250 to 500°C;
- c) a feed gas pressure in the range of 0.8 to 70 bar;
- d) an gas hourly space velocity of 1000 to 50000 h⁻¹; and
- e) an concentration of H₂/CO in the initial gas mixture in the range of 0.25 to 5.

20

2. The process according to claim 1, characterized in that

25

the catalytic active component is nickel and/or a nickel compound, preferably a mixture of nickel and nickel oxide, disposed on an ceramic carrier, such as Al₂O₃, TiO₂, SiO₂ or Y₂O₃ or mixtures thereof.

30

3. The process according to claim 2, characterized in that

the content of the catalytically active component is in the range of 20 to 80 weight%, preferably 40 to 60 weight%, as compared to the weight of the catalyst particles.

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4. The process according to claim 1, 2 or 3,
characterized in that
the size of the catalyst particles is in the range of 10 to
5 1000 μm , preferably in the range of 100 to 500 μm .
5. The process according to anyone of the preceding claims,
characterized in that
the feed gas mixture comprises aromatic hydrocarbons, such as
10 benzene, toluene and naphthalene, in the range of less than 10
Vol%, preferably less than 5 vol%.
6. The process according to anyone of the preceding claims,
characterized in that
15 the gas hourly space velocity is in the range of 2000 to 10000
 h^{-1} , the temperature is in the range of 340 to 400°C and the
gas pressure is in the range of 1 bar.
7. The process according to anyone of the preceding claims,
20 characterized in that
a mean residence time of the feed gas mixture in the fluidized
bed catalyst is in the range of 0.1 to 5 sec., preferably 0.2
to 1 sec.
- 25 8. The process according to anyone of the preceding claims,
characterized in that
the content of H_2/CO in the feed gas mixture is in the range of
0.8 to 2.

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Abstract

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The present invention discloses a process for the synthetic generation of methane from a feed gas mixture comprising carbon monoxide, hydrogen and water vapour and optionally aromatic hydrocarbons; said process comprising the steps of:

- 10 a) bringing the feed gas mixture in contact with a fluidized bed catalyst having catalyst particles which comprise as catalytic active component a metal and/or a metal compound or a mixture thereof under the circumstances of:
- b) an elevated temperature in the range of 250 to 500°C;
- 15 c) a feed gas pressure in the range of 0.8 to 70 bar;
- d) an gas hourly space velocity of 1000 to 50000 h⁻¹; and
- e) an concentration of H₂/CO in the initial gas mixture in the range of 0.25 to 5.

- 20 The afore-mentioned process allows to catalytically convert hydrogen and carbon monoxide effectively in the fluidized bed catalyst which avoids an advanced deactivation of the catalyst material and therefore delivers a high activity of the catalytic active components in the process. Both thermo-
- 25 chemical reactions, the endothermic reformation of higher hydrocarbons, i.e. aromatic hydrocarbons, and the exothermic methane generation, themselves synergetic fertilize which in fact tremendously increases the tolerance of this process against the content of higher hydrocarbons in the feed gas
- 30 mixture, such a the raw synthesis gas of a wood gasification process, by simultaneously enhancing the robustness of the catalytic activity and selectivity of the catalyst particles.